Non Dimensionalisation of Basic Equation

- You have seen the Buckingham Π method to non-dimensionalise the relations or form non-dimensional relation for various experimental data.
- You also developed or came up with non-dimensional numbers or parameters.
- In today's class, we will see the non-dimensionalisation of the basic equations and see whether we can get some non-dimensional numbers.

Recall for an incompressible fluid (mainly liquid), the continuity equation was:

 $\vec{\nabla}.\vec{v} = 0 \qquad (\text{vector form})$ $\frac{\partial v_i}{\partial x_i} = 0 \qquad (\text{index form})$ $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \qquad (\text{expanded form})$

Also for the incompressible liquid, the momentum equation was:

$$\rho \left[\frac{\partial \vec{v}}{\partial t} + u \frac{\partial \vec{v}}{\partial x} + v \frac{\partial \vec{v}}{\partial y} + w \frac{\partial \vec{v}}{\partial z} \right] = \rho \vec{g} - \vec{\nabla} p + \mu \nabla^2 \vec{v} \qquad \text{(Vector Form)}$$
$$\rho \left[\frac{\partial v_i}{\partial t} + v_j \frac{\partial (\rho v_i)}{\partial x_j} \right] = \rho g_i - \frac{\partial p}{\partial x_i} + \mu \frac{\partial^2 v_i}{\partial x_j \partial x_j}$$

The typical boundary conditions used to solve fluid flow are:

- \blacktriangleright Fixed solid surface, i.e. $\vec{v} = 0$
- > Inlet or outlet flow, known. i.e. given \vec{v} , p, etc.
- Free surface, such that $p_{liquid} = p_{atm}$ or water surface.

For incompressible liquids, the variables and parameters are now: $\rho = \text{constant}$ (A parameter)

p, \vec{v} , x, y, z, t are the variables present in the equation.

- ➤ The basic dimensions are M, L, T
- > We need to non-dimensionalise the variables.
- ➢ For that, we need to fix some reference values.

Let the reference velocity be v and reference length L (Reference value means they are not variables and they are known values apriori).

The reference values can be eg: Inlet or Upstream velocity U, it can be diameter of immersed body, or diameter of pipe, or length of aerofoil, etc.

Define Non-dimensional variables:

$$\vec{v}^* = \frac{\vec{v}}{U}$$

Please note that we will be using * as superfix on each variable to show that it is a non-dimensional variable.

$$u^{*} = \frac{u}{U}, \quad v^{*} = \frac{v}{U}, \quad w^{*} = \frac{w}{U}$$

$$x^{*} = \frac{x}{L}, \quad y^{*} = \frac{y}{L}, \quad z^{*} = \frac{z}{L}$$

$$\nabla^{*} = \hat{i} \frac{\partial}{\partial x^{*}} + \hat{j} \frac{\partial}{\partial y^{*}} + \hat{k} \frac{\partial}{\partial z^{*}}$$
or
$$\nabla^{*} = L\hat{i} \frac{\partial}{\partial x} + L\hat{j} \frac{\partial}{\partial y} + L\hat{k} \frac{\partial}{\partial z}$$

$$= L\left[\hat{i} \frac{\partial}{\partial x} + \hat{j} \frac{\partial}{\partial y} + \hat{k} \frac{\partial}{\partial z}\right]$$
or
$$\nabla^{*} = L\nabla$$

$$t^{*} = L\nabla$$

$$t^{*} = t \frac{U}{L}$$

$$p^{*} = \frac{p + \rho gz}{\rho u^{2}}$$

(Note: ∇ * is an operator) *p** is computed with respect to piezo metric head (*p*+ ρgz) in the numerator.

Note : ρ , U, L are constant.

Therefore, $\frac{\partial u}{\partial x} = \frac{\partial (Uu^*)}{\partial (Lx^*)} = \frac{U}{L} \frac{\partial u^*}{\partial x^*}$ Similarly,

$$\frac{\partial v}{\partial y} = \frac{\partial (Uv^*)}{\partial (Ly^*)} = \frac{U}{L} \frac{\partial v^*}{\partial y^*}$$
$$\frac{\partial w}{\partial z} = \frac{\partial (Uw^*)}{\partial (Lz^*)} = \frac{U}{L} \frac{\partial w^*}{\partial z^*}$$

The continuity equation can be expressed in non-dimensional form as:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

$$\frac{U}{L} \left[\frac{\partial u^*}{\partial x^*} + \frac{\partial v^*}{\partial y^*} + \frac{\partial w^*}{\partial z^*} \right] = 0$$

$$\vec{\nabla}^* \cdot \vec{v}^* = 0$$
(1)

The **momentum equation** can be non dimensionalised:

Note :
$$\frac{\partial \vec{v}}{\partial t} = \frac{\partial (U\vec{v}^*)}{\partial (\frac{Lt^*}{U})} = \frac{U^2}{L} \frac{\partial \vec{v}^*}{\partial t^*}$$

The left side of the Naiver – Stokes momentum equation

$$\rho \left[\frac{U^2}{L} \left(\frac{\partial \vec{v} *}{\partial t *} \right) + \left(Uu * \right) \frac{U}{L} \frac{\partial u *}{\partial x *} + \left(Uv * \right) \frac{U}{L} \frac{\partial v *}{\partial y *} + \left(Uw * \right) \frac{U}{L} \frac{\partial w *}{\partial z *} \right]$$

$$= \rho \frac{U^2}{L} \left[\frac{\partial \vec{v} *}{\partial t *} + u * \frac{\partial \vec{v} *}{\partial x *} + v * \frac{\partial \vec{v} *}{\partial y *} + w * \frac{\partial \vec{v} *}{\partial z *} \right]$$

$$= \rho \frac{U^2}{L} \left[\frac{\partial \vec{v} *}{\partial t *} + (\vec{v} * . \nabla *) \vec{v} * \right]$$

$$= \rho \frac{U^2}{L} \left[\frac{d \vec{v} *}{d t *} \right]$$

The non dimensionalisation of RHS of Naiver - Stokes momentum equation

(Recall
$$p* = \frac{p + \rho gz}{\rho u^2}$$
)

You can derive yourself and check.

You will get

$$\rho \vec{g} - \vec{\nabla} p + \mu \nabla^2 \vec{v} = -\rho \frac{U^2}{L} \nabla^* p^* + \frac{\mu}{\rho UL} \left(\rho \frac{U^2}{L}\right) \nabla^{*2} (\vec{v}^*)$$

$$\frac{d\vec{v}^*}{dt^*} = -\nabla^* p^* + \frac{\mu}{\rho UL} \nabla^{*2} \left(\vec{v}^* \right)$$
⁽²⁾

Equation (2) is non-dimensional form of linear momentum equation.

You can see from equation (2), there are non-dimensional number like Reynolds number present ij the expression. Therefore,

$$\frac{d\vec{v}^*}{dt^*} = -\nabla^* p^* + \frac{1}{R_e} \nabla^{*2} (\vec{v}^*)$$

For boundary conditions, if $\vec{v} = 0$ Then non-dimensional form, $\vec{v}^* = 0$

(For fixed solid surface)

For inlet and outlet known values, you can provide p^*, \vec{v}^* . For free surface,

$$z^* = \eta^* \text{ or } w^* = \frac{d\eta^*}{dt}$$
$$p^* = \frac{p_{atm}}{\rho u^2} + \frac{gL}{U^2} z^*$$

The free surface pressure condition has non-dimensional numbers (or parameter):

Euler Number , Eu =
$$\frac{p_{atm}}{\rho u^2}$$

Froude Number, $Fr^2 = \frac{U^2}{gL}$

Similarly, in fluid mechanics, you will come up with various such types of non-dimensional parameters:

I. Reynolds Number,
$$R_e = \frac{\rho UL}{\mu}$$

II. Mach Number, $Ma = \frac{U}{a}$
III. Froude Number, $Fr = \frac{U}{\sqrt{gL}}$
IV. Weber Number, $We = \frac{\rho U^2 L}{\gamma}$
V. Cavitation Number, $C_a = \frac{p - p_v}{\rho U^2}$